

# Downers Grove Sanitary District Wastewater Treatment Center

## Nutrient Study

Nick Menninga, P.E., BCEE

Derek Wold, P.E., BCEE

Amanda Poole, P.E.

January 23, 2014

# OUTLINE



- ✓ Background
- ✓ Study Purpose and Scope
- ✓ Chemical Phosphorus Removal
- ✓ Biological Phosphorus Removal
  - Computer Model of Plant Process
  - A/O Process Evaluation
- ✓ Recommendations
- ✓ Future Considerations

# BACKGROUND: DRAFT NPDES CONDITION

- NPDES permit is currently expired
- Draft NPDES Permit Special Condition
  - *Maintain membership with DRSCW*
  - *Phosphorus feasibility study*
    - *Improvements to meet 1.0 mg/L TP*
    - *Interim measures to reduce TP*

# SCOPE OF WORK

- ✓ Goal: satisfy NPDES Condition
- ✓ Evaluate improvements to meet a TP Limit of 1 mg/L
  - Interim
  - Permanent
- ✓ Phosphorus Removal Only
- ✓ Excess Flow Not Evaluated



# Background: DGSD overview

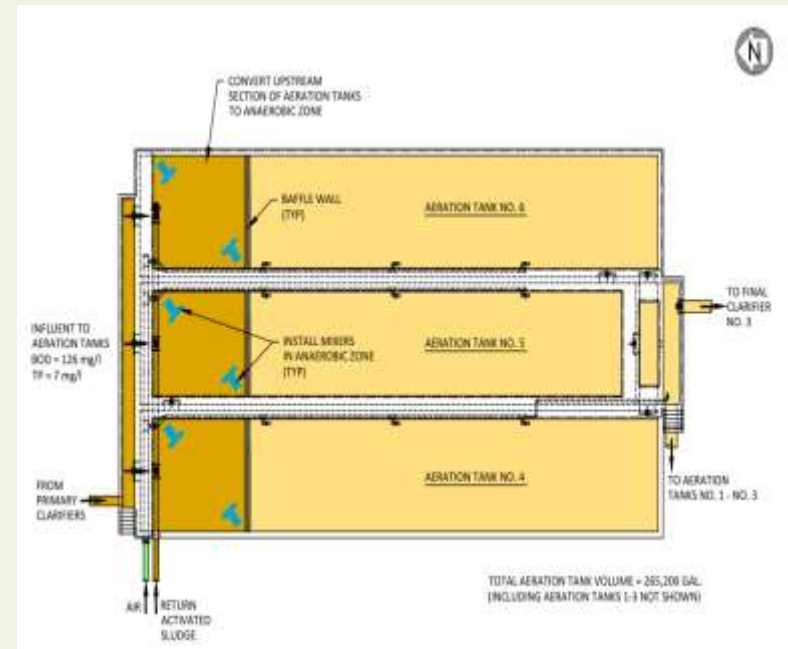
- 11/22 MGD average/peak full treatment capacity
- Primary clarification
- Single-stage nitrification
- Tertiary sand filtration
- Anaerobic digestion
- Sludge dewatering and aging
- Excess flow primary and disinfection to 110 MGD total

# OPTIONS FOR TOTAL PHOSPHORUS REMOVAL

Two options for phosphorus removal:



Chemical



Biological

# CHEMICAL PHOSPHORUS REMOVAL

## Chemical Precipitation of Phosphorus

- Advantages – simple process
- Disadvantages – costly operation, less sustainable
- Capital Costs: \$500,000
- Annual O&M Costs: \$540,000 total
  - \$415,000 chemicals
  - \$125,000 sludge



# BIOLOGICAL PHOSPHORUS REMOVAL

## Biological Nutrient Removal

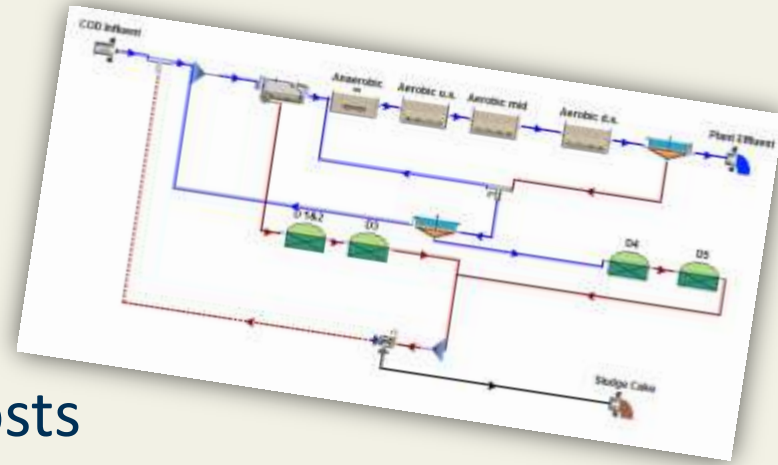
- Advantages – Lower O&M costs, more sustainable
- Disadvantages – Less reliable, still under development
- Costs – Depend on design goals.
  - *Interim project in existing footprint: \$500,000 capital, \$10,000 annual O&M*
  - *1 mg/l limit, \$3 million capital, \$20,000 annual O&M. Could be lower with on-site R&D.*



# BIOLOGICAL PHOSPHORUS REMOVAL

Challenge: How to control the cost of EBPR?

- Biowin Model
- Substrate availability of VFAs
- Minimize capital and O&M costs
- Goal: determine optimum combination of biological and/or chemical addition
- Capacity and nitrification issues



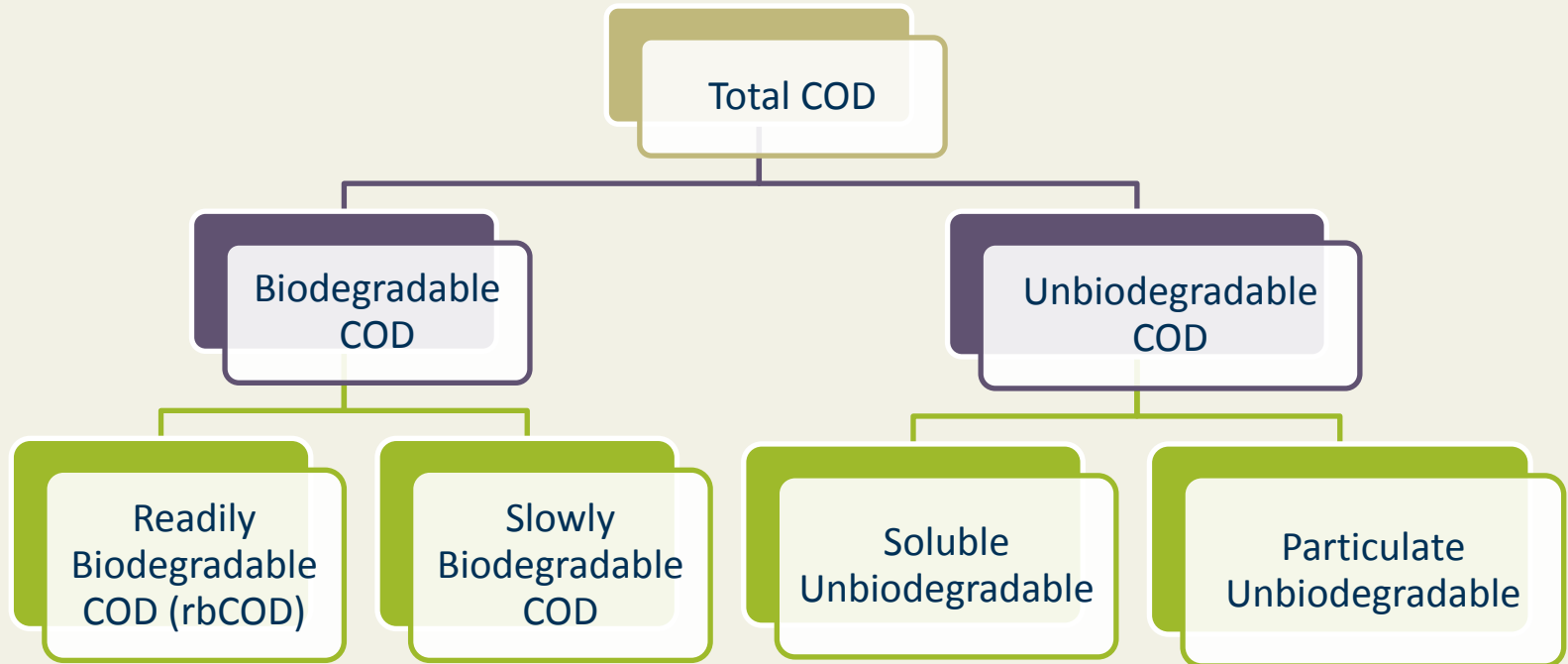
# BIOLOGICAL PHOSPHORUS REMOVAL

## Biowin Model

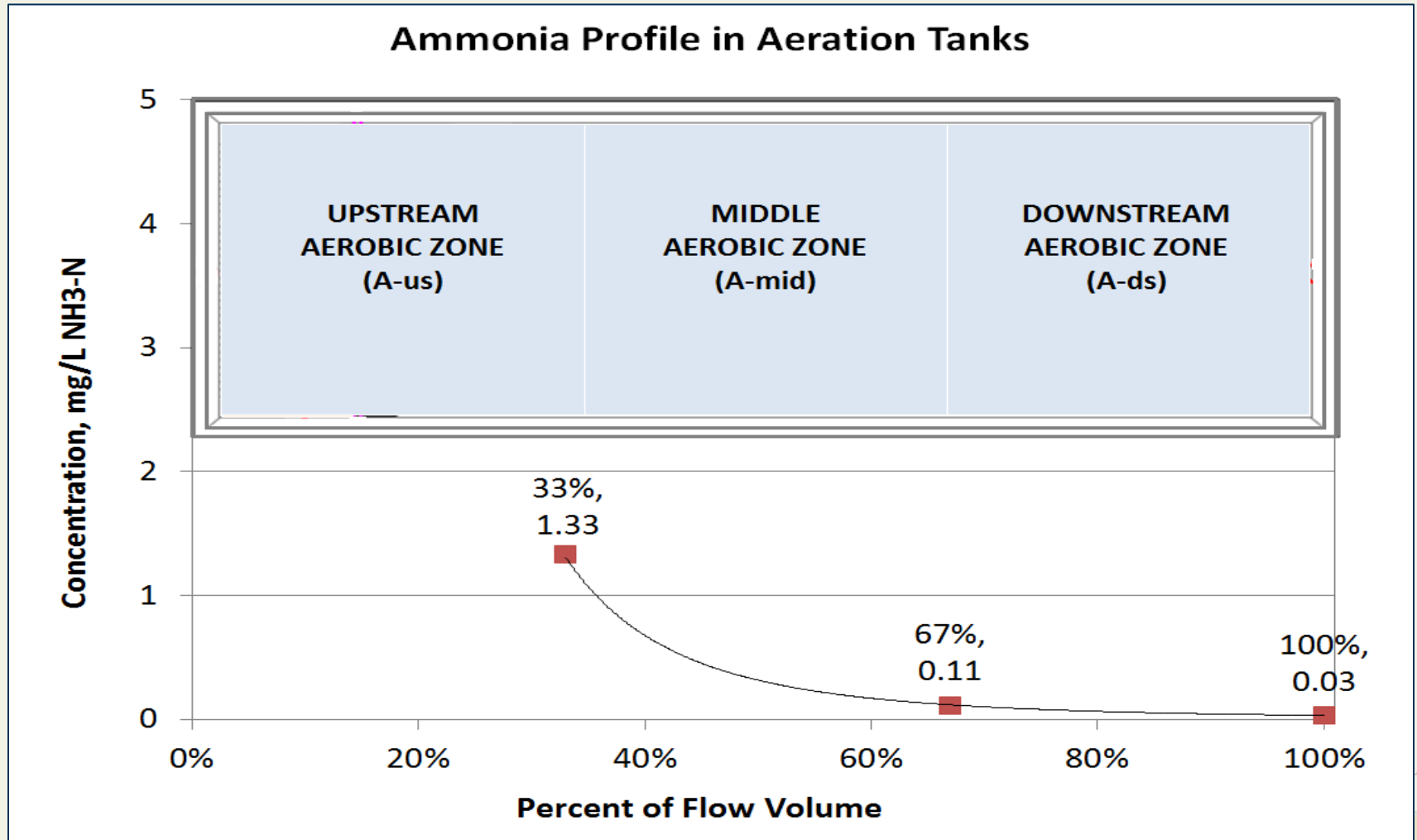
- Establish a baseline of existing operation
  - Collect data
  - Calibrate model
  - Verify model
- Model EBPR Scenarios
  - A/O Selected from several options

# BIOLOGICAL PHOSPHORUS REMOVAL

## rbCOD Sampling



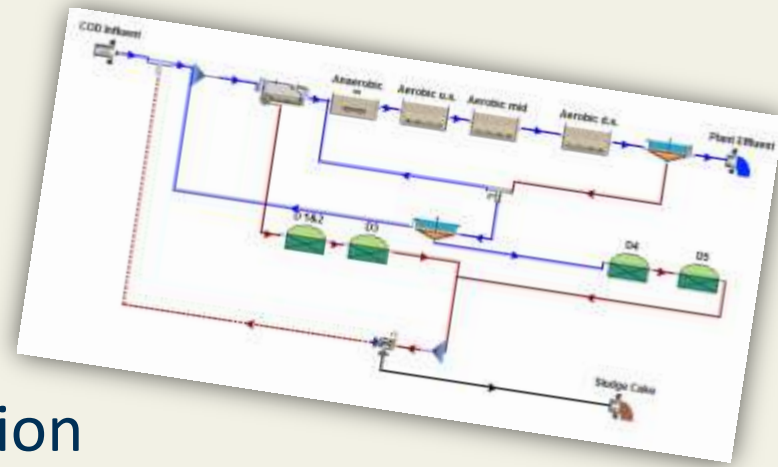
# BASELINE MODEL RESULTS



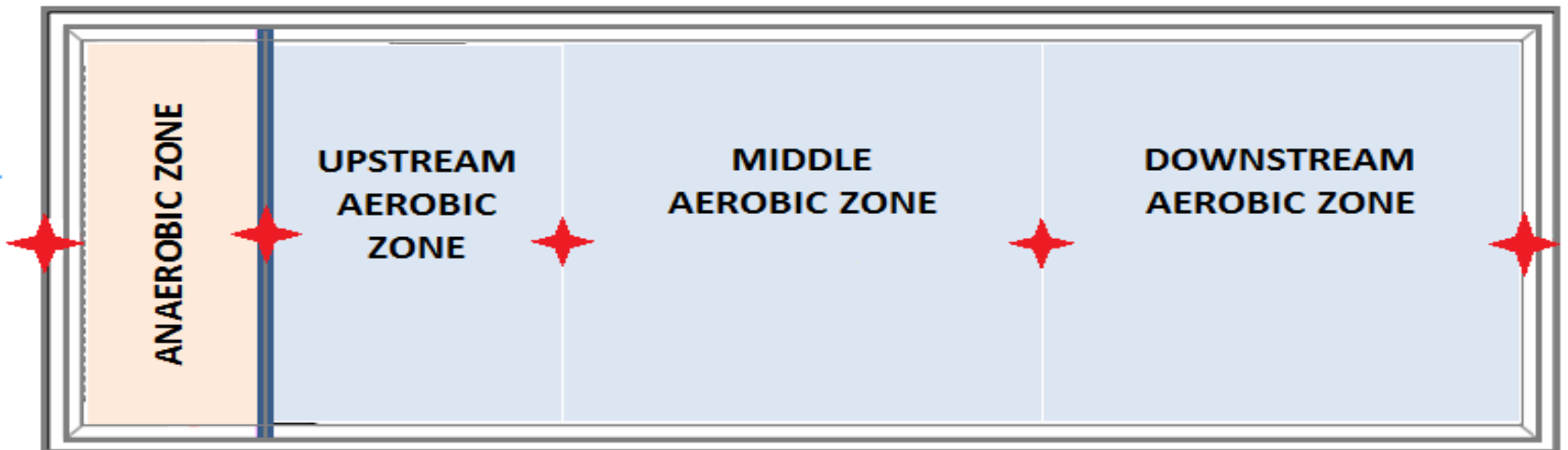
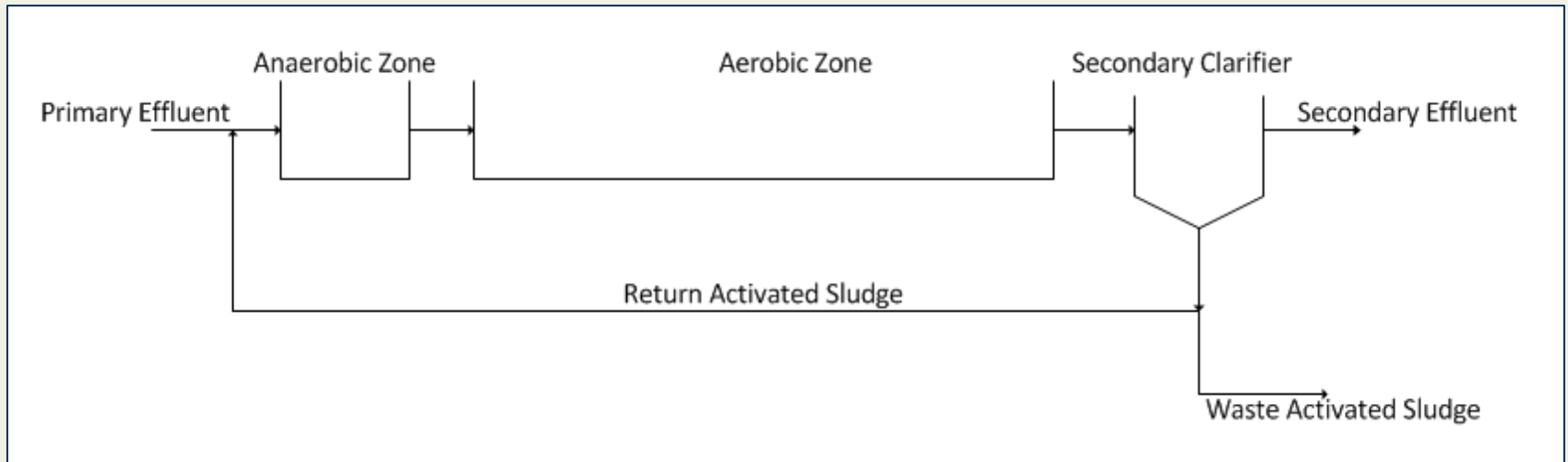
# BIOLOGICAL PHOSPHORUS REMOVAL

## A/O Process

- Define
- Simplest BioP Process
- Effective for TP
- Maximizes space for nitrification
- Can be used as a swing zone in the future

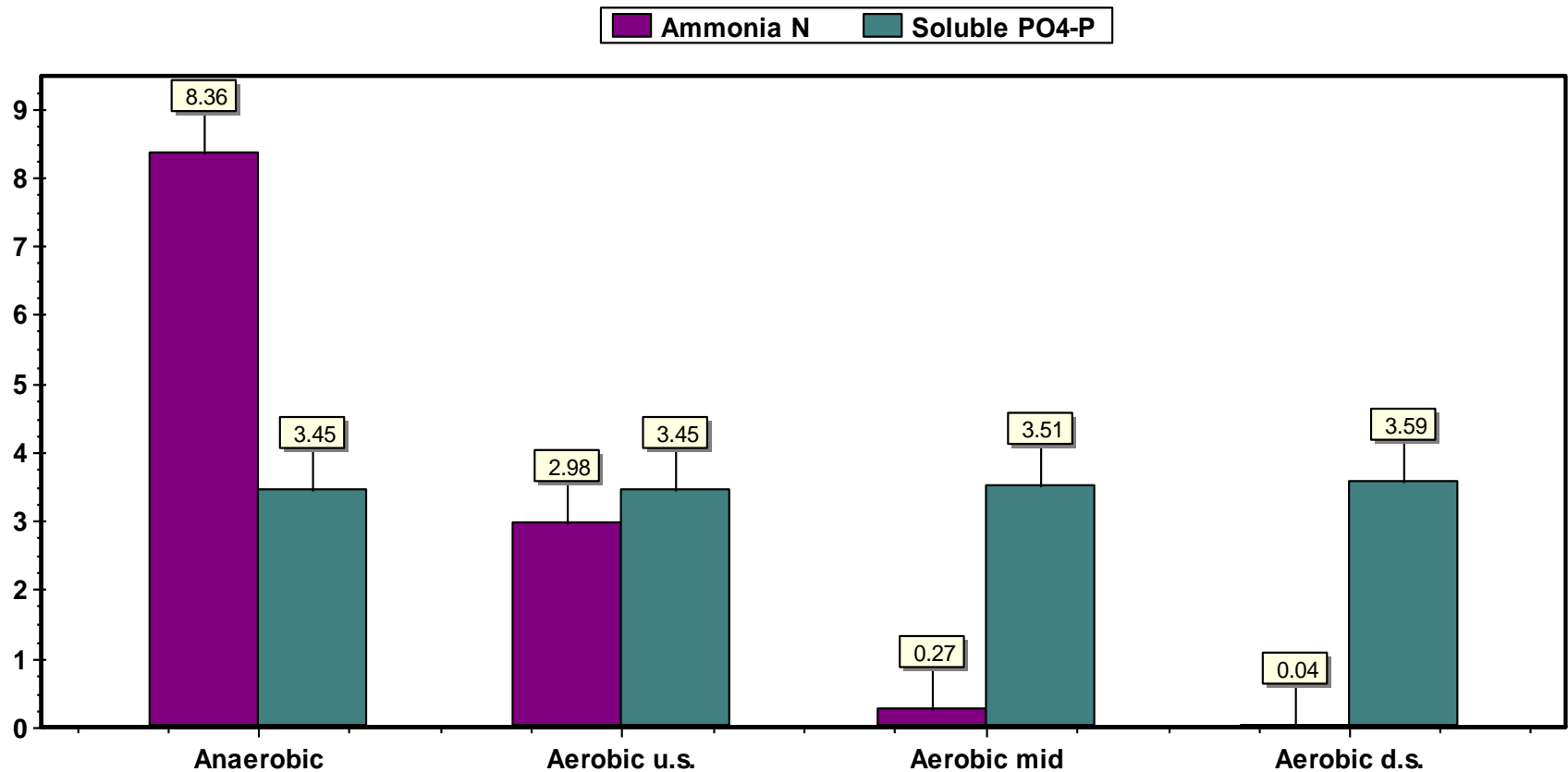


# BIOLOGICAL PHOSPHORUS REMOVAL: A/O PROCESS



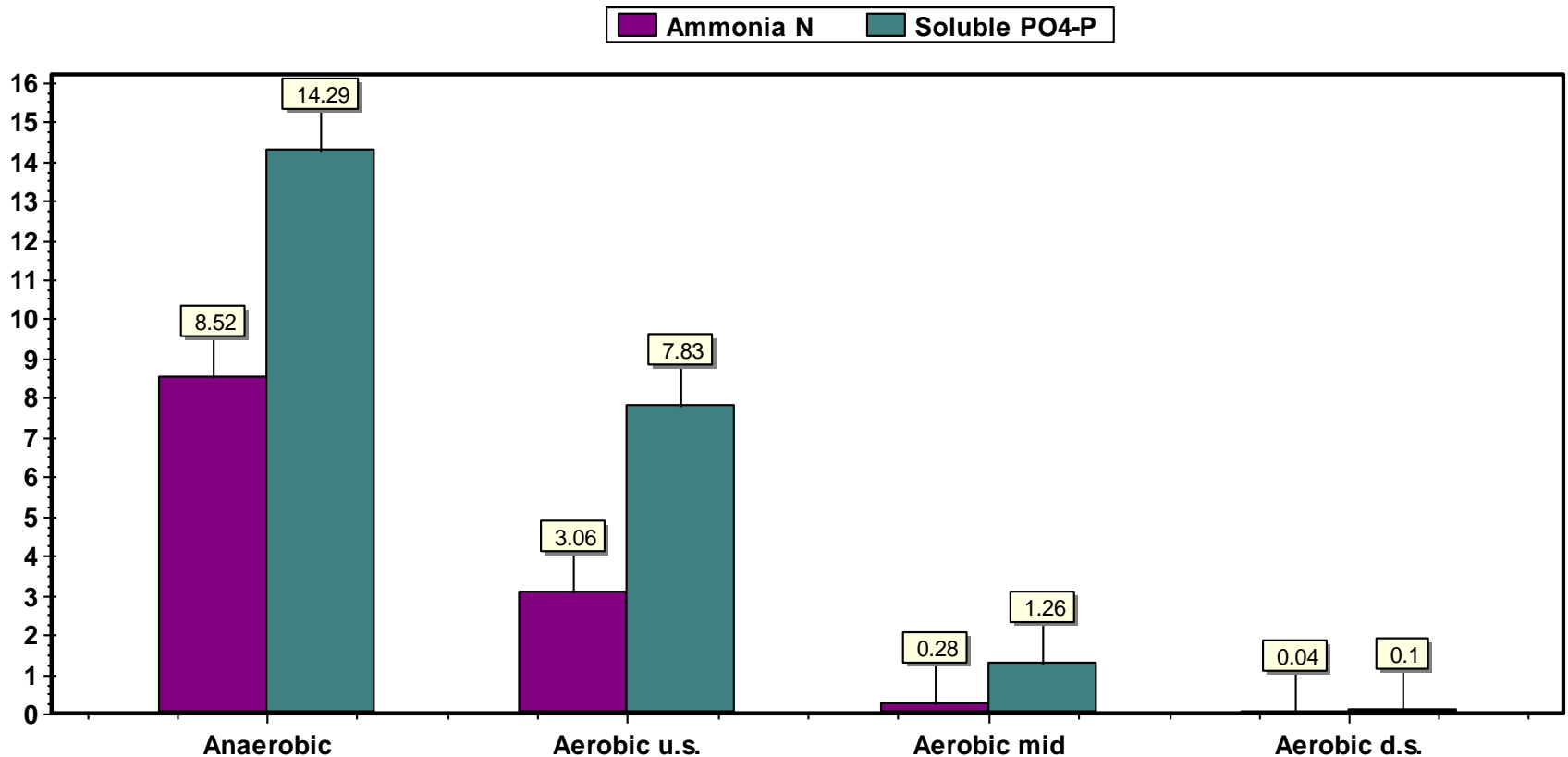
# BIOLOGICAL PHOSPHORUS REMOVAL: A/O PROCESS

A/O (no VFA Supplementation); 20°C, 10d SRT



# BIOLOGICAL PHOSPHORUS REMOVAL: A/O PROCESS

A/O with VFA Supplementation (8,400 ppd); 20°C, 10d SRT





# BIOLOGICAL PHOSPHORUS REMOVAL

## Modeling Results

- Model Performance

Process	A/O	A2/O
TP	< 0.45 mg/L	< 0.5 mg/L
TN	< 11 mg/L	< 7 mg/L
NH <sub>3</sub> -N	< 0.5 mg/L	< 2 mg/L

# BIOLOGICAL PHOSPHORUS REMOVAL

## VFA Supplementation Options:

- Carbon Addition
- Primary Sludge Fermentation

# RECOMMENDATIONS

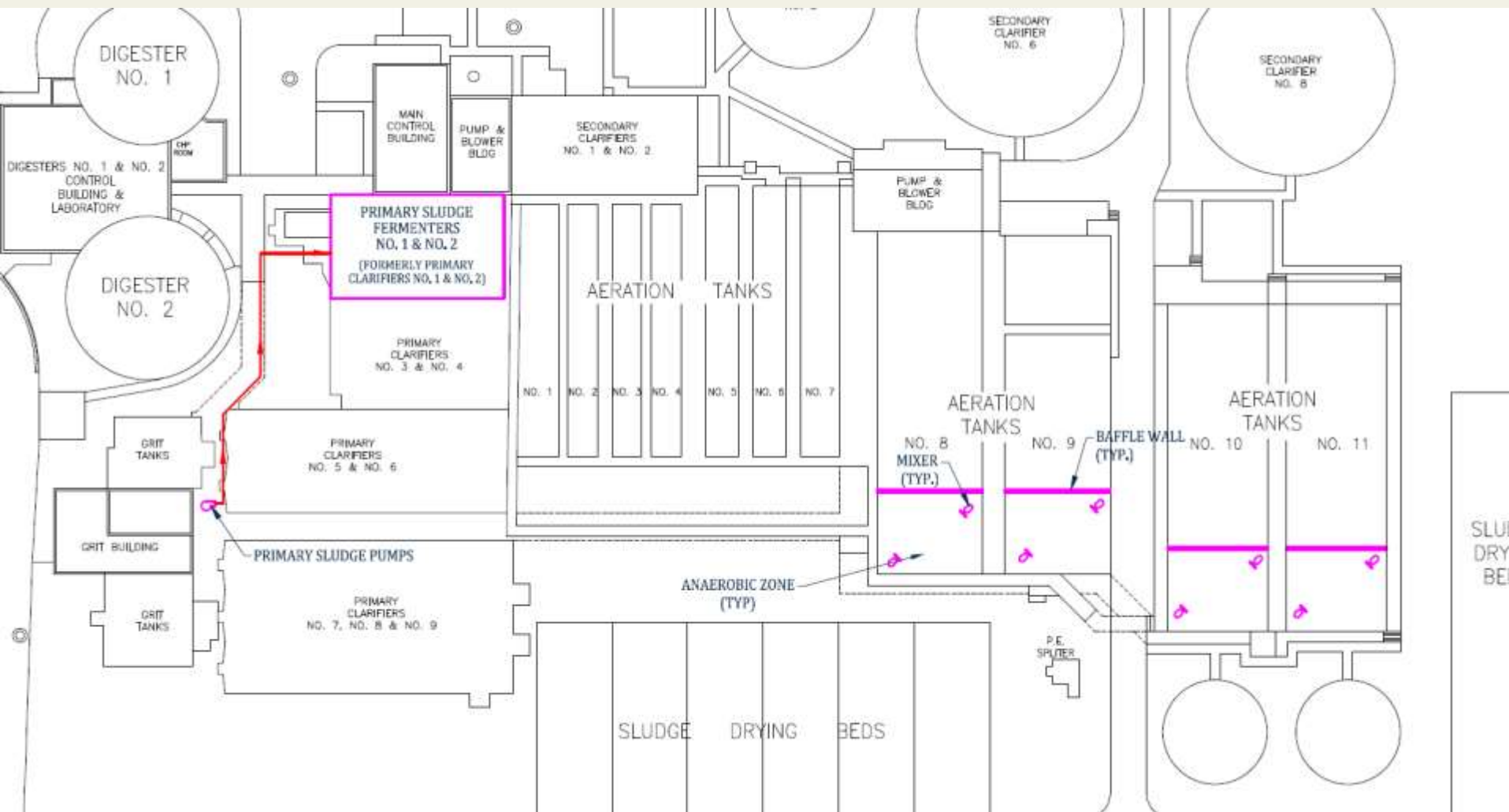
Part / Scope	Costs	
	Capital*	Annual
Phase 0: Primary Sludge Fermentation Trial	-	-
Phase 1: Convert to an A/O Process	\$593,000	\$10,750
Phase 2: Convert Primary Clarifiers No. 1 & 2 to Primary Sludge Fermenters	\$1.84 million	\$8,900**
Phase 3: Backup Chemical Feed System	\$575,000	N/A
<b>Total</b>	<b>\$3.01 million</b>	<b>\$19,650</b>

**NEEDED TO MEET 1 MG/L?**

\* Capital costs include engineering and a 10% contingency.

\*\* The costs for Phase 2 assume sufficient VFAs are produced for EBPR to meet an effluent phosphorus concentration of 1mg/L. Otherwise, the District should re-evaluate chemical polishing versus dedicated primary sludge fermentation tanks.

# RECOMMENDATIONS: Phase 1 and 2



# FUTURE CONSIDERATIONS

If primary sludge fermentation does not produce sufficient VFAs

- Re-evaluate the cost-effectiveness of
  - VFA addition with Primary Sludge Fermentation
  - Chemical Phosphorus Removal
    - Polishing and Full Treatment
- Struvite Harvesting

# QUESTIONS

Nick Menninga, P.E.  
[nmenninga@dgsd.org](mailto:nmenninga@dgsd.org)

Derek J. Wold, P.E.  
[dwold@baxterwoodman.com](mailto:dwold@baxterwoodman.com)